Adjoint Implementation of Rosenbrock Methods Applied to Variational Data Assimilation Problems

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ADJOINT IMPLEMENTATION OF ROSENBROCK METHODS

Abstract.

In the past decade the variational method has been successfully applied in data assimilation problems for atmospheric chemistry models [10, 11, 12]. In 4D-var data assimilation a minimization algorithm is used to find the set of control variables which minimizes the weighted least squares distance between model predictions and observations over the assimilation window. Using the adjoint method, the gradient of the cost function can be computed fast, at the expense of few function evaluations, making the optimization process very efficient. For large scale models, the high storage requirements and the difficulty to implement the adjoint code when sophisticated integrators are used to solve the stiff chemistry make the assimilation a very intensive computational process. If the sparse structure of the chemical models is carefully exploited, Rosenbrock methods have been proved to be reliable chemistry solvers due to their outstanding stability properties and conservation of the linear invariants of the system. In this paper we present an efficient implementation of the adjoint code for the Rosenbrock type methods which can reduce the storage requirements of the forward model and is suitable for automatization. The adjoint code is completely generated using symbolic preprocessing and automatic differentiation tools which allows for flexibility and requires minimal user intervention.

1. INTRODUCTION

Consider a 3D atmospheric transport-chemistry model given by the system of differential equations:

$$\frac{\partial}{\partial t} \mathbf{c}_i = -\nabla \cdot (\mathbf{u} \mathbf{c}_i) + \nabla \cdot (\mathbf{K} \cdot \nabla \mathbf{c}_i) + f_i(\mathbf{c}) + E_i, \ i = \overline{1, S}. \tag{1.1}$$

The initial condition is $c(t_0) = c_0$ and appropriate boundary values are prescribed. The solution $c(t,x,y,z) \in R^S$ of problem (1.1) represents the concentration vector of the chemical species in the model, \mathbf{u} is the wind field and \mathbf{K} is the eddy diffusivity tensor; the chemical reactions are modeled by the nonlinear stiff terms $f_i(\mathbf{c}) = P_i(\mathbf{c}) - D_i(\mathbf{c})c_i$, with $P_i(\mathbf{c})$, $D_i(\mathbf{c})$ the chemical production and destruction terms; E_i represents the source term, and depositions are modeled as a boundary condition at earth's surface:

$$-\mathbf{n}_h \cdot (\mathbf{K} \cdot \nabla \mathbf{c}_i) = Q_i - v_i \mathbf{c}_i$$

with \mathbf{n}_h the inward vector normal to the earth's surface, Q_i and v_i the surface emission rate and deposition velocity of species i, respectively. Space and time dependence is assumed for all terms, but for simplicity the explicit notation is omitted. A complete model description is given in [6]. We will refer to problem (1.1) as the forward model and $\mathbf{c}(t), t \in [t_0, T]$ will represent the "forward trajectory". The forward trajectory is determined by the values of the parameters in (1.1) and typical choices for the set of control variables in data assimilation are the boundary values, initial concentrations, emissions and deposition rates. When the identifying parameters are distributed in the space time domain, instabilities and nonuniqueness problems may appear for the inverse modeling techniques (in addition to those given by the nonlinear structure of the model). A general framework for adjoint parameter estimation and a discussion of the parameter identifiability problem is presented in [23]. For the purpose of this paper, we consider the 4D variational data assimilation problem associated to (1.1) with the set of control variables given by the initial state of the model, c_0 . Under suitable assumptions, problem (1.1) has an unique solution and we can view this solution as a function of the initial conditions, $\mathbf{c} = \mathbf{c}(t, x, y, z, \mathbf{c}_0)$.

If space discretization is applied to problem (1.1) on a grid (N_x, N_y, N_z) , the resulting ODE system of dimension $N = S \times N_x \times N_y \times N_z$ is:

$$\begin{cases} \frac{d\mathbf{C}}{dt} = F_A(c) + F_D(c) + F_R(c) \\ c(t_0) = c_0 \end{cases} \tag{1.2}$$

where F_A represents the advection and horizontal diffusion, F_D is the vertical diffusion which may introduce additional stiffness, and the reaction terms are given by F_R . The source and sink terms may be included in F_D [6] or in the chemistry operator F_R [3, 33]. We assume that a previous analysis provides a "background estimate" c^b of c_0 with the error covariance matrix \mathbf{B} , and measurements c_k^o , k=1,m of the concentrations at moments t_k are scattered over the interval $[t_0,T]$. The errors in measurements and model representativeness are given by the covariance matrices \mathbf{R}_k , k=1,m. The covariance matrices \mathbf{B} and \mathbf{R}_k are symmetric and positive definite (if they do not contain null or infinite variances, or perfect correlations, [32]) such that \mathbf{B}^{-1} , \mathbf{R}_k^{-1} are well defined. In practice \mathbf{B} , \mathbf{R}_k are often taken diagonal which corresponds to the assumption that there is no spatial and chemical correlation in the background errors, and measurement and model errors are uncorrelated in space and time. The 4D-var data assimilation finds an initial state c_0 that minimizes the distance between the model predictions and observations expressed by the cost function:

$$\mathcal{F}(\mathbf{c}_0) = \frac{1}{2}(\mathbf{c}_0 - \mathbf{c}^b)^T \mathbf{B}^{-1}(\mathbf{c}_0 - \mathbf{c}^b) + \frac{1}{2} \sum_{k=1}^m (\mathbf{c}_k - \mathbf{c}_k^o)^T \mathbf{R}_k^{-1}(\mathbf{c}_k - \mathbf{c}_k^o)$$
(1.3)

The quality of the assimilation results depends on several factors such as: availability and spatial-temporal distribution of measurements, accuracy of the background estimate, length of the assimilation window, errors in measurements and model representativeness. The existence of multiple local minima of the functional \mathcal{F} may lead to ambiguous assimilation results. This analysis is beyond the goal of this paper, and details can be found in [10, 12, 18] and the references therein.

Most of the powerful optimization techniques require the evaluation of the gradient $\nabla_{c_0} \mathcal{F}$ of the cost function. In a comprehensive atmospheric chemistry model the dimension of

the vector c_0 can easily be of order 10^6 which make the optimization a very expensive computational process.

In the variational approach one computes the gradient of the functional \mathcal{F} by using the "adjoint method". Since for nonlinear problems (such as 1.1,1.2) the corresponding adjoint equations depend on the forward trajectory, the computational cost and the complexity of the adjoint implementation are significantly increased as compared with linear problems. The general theory of adjoint equations is described in [20, 21] and the derivation of the adjoint model for the continuous and discrete case is given in [12, 31]. Below we outline the basic ideas. The gradient of the cost function is:

$$\nabla_{c_0} \mathcal{F}(\mathbf{c}_0) = \mathbf{B}^{-1}(\mathbf{c}_0 - \mathbf{c}^b) + \sum_{k=1}^m \left(\frac{\partial \mathbf{c}_k}{\partial \mathbf{c}_0}\right)^T \mathbf{R}_k^{-1}(\mathbf{c}_k - \mathbf{c}_k^o)$$
(1.4)

Using the chain rule in its transpose form $\left(\frac{\partial C_k}{\partial C_0}\right)^T = \left(\frac{\partial C_{k-1}}{\partial C_0}\right)^T \left(\frac{\partial C_k}{\partial C_{k-1}}\right)^T$ we can deduce the algorithm to compute the necessary gradient:

Step1. Initialize gradient = 0

Step 2.
$$for k = m, 1, -1 do$$

$$gradient = \left(\frac{\partial C_k}{\partial C_{k-1}}\right)^T \left[\mathbf{R}_k^{-1}(c_k - c_k^o) + gradient\right]$$

Step3.
$$gradient = \mathbf{B}^{-1}(c_0 - c^b) + gradient$$

The main advantage of the adjoint method is that explicit computation of the Jacobian matrices $\frac{\partial C_k}{\partial C_{k-1}}$ is avoided and the matrix-vector products can be computed directly at Step 2. For the theory and actual implementation of the adjoint computations the reader should consult [14, 15, 22]. Since the algorithm described above requires the values of c_k in reverse order, these values need to be stored from a previous run or recomputed. Moreover, in practice the measurements are usually sparse and the value of c_k is obtained from c_{k-1} with a sequence of steps $c_{k-1} \to c_k^1 \to \ldots \to c_k^s \to c_k$. The computational trade-off is then between allocating a huge amount of memory to store the states of the system during the forward run, or frequent recomputations which increase the running time of the code. If

an explicit numerical method is used to solve the stiff chemistry part of problem (1.2) then the "trajectory" from c_{k-1} to c_k may become very long, increasing the cost of the adjoint code. On another hand, if an implicit method is used then the adjoint computations may become complicated. Ideally one would like a method capable of taking large stepsize and an efficient adjoint implementation.

2. OPERATOR SPLITTING

A popular way to solve problem (1.2) is to use operator splitting, which has the advantage that processes such as advection, vertical diffusion and chemical reactions can be treated with different numerical methods. In a second order accurate Strang splitting [30] approach with the time step $h = t_{n+1} - t_n$, the solution c_{n+1} is obtained from c_n as follows:

$$c_{n+1} = \overline{F}_A\left(t_{n+\frac{1}{2}}, \frac{h}{2}\right) \overline{F}_D\left(t_{n+\frac{1}{2}}, \frac{h}{2}\right) \overline{F}_R(t_n, h) \overline{F}_D\left(t_n, \frac{h}{2}\right) \overline{F}_A\left(t_n, \frac{h}{2}\right) c_n \quad (2)$$

where the operators \overline{F} are defined by the numerical method used to solve the corresponding processes. If \overline{J} denotes the $N \times N$ Jacobian matrix associated to \overline{F} , the adjoint algorithm to compute the gradient (1.4) of the cost function requires products of the form $\overline{J}^T u$, with u an arbitrary seed vector. Since for large systems constructing the adjoint code by hand can be a frustrating process, automatic tools have been developed [14, 24]. Automatic implementation allows also for flexibility, such that if the model is modified minimal user intervention is required.

Usually \overline{F}_A is defined by an explicit method and may be nonlinear (e.g. if a flux-limiter is applied for positivity [17, 35]), \overline{F}_D is linear, defined by a (semi-) implicit method. The products $\overline{J}_A^T u$ and $\overline{J}_D^T u$ can be then efficiently computed using an automatic adjoint compiler. Coleman et al.[8] present an "extended Jacobian" framework to exploit the sparsity of a finite difference scheme, which leads to efficient computations of the adjoint products when automatic differentiation is applied on the finite difference stencils.

The operator \overline{F}_R is highly nonlinear, given by a stiff numerical method, and the computation of $\overline{J}_R^T u$ needs special consideration. A key element for the efficient implementation of

the forward code is to exploit the sparse structure of the chemical model. Sparse computations must be then performed as well during the backward integration. Since the adjoint method requires several integrations of the direct model, the storage of (part of) the forward trajectory and the computation of the $(jacobian)^T \cdot vector$ products, the performance of the adjoint model is dominated by the implementation of the direct and adjoint method used in the chemistry integration which takes in practice as much as 90% of the CPU time. Fisher and Lary[12] show the adjoint computations for the adaptive-timestep Bulirsch-Stoer method, and Elbern and Schmidt[10] use the adjoint model for a quasi steady state approximation (QSSA) scheme. In the next section we present the adjoint formulas for a general 2-stage Rosenbrock method and an efficient implementation which is suitable for automatization. The L-stable method ROS2 we obtain as a particular case was applied for the chemistry integration in the forward 3D model LOTOS [3] in the context of various types of operator splitting and using approximate Jacobians (as a W-method). Extension to a general s-stage method [16] is straightforward.

3. ADJOINT COMPUTATIONS AND IMPLEMENTATION FOR A 2-STAGE ROSENBROCK METHOD

i) Derivation of the adjoint formulas. We consider now the problem

$$\begin{cases} \frac{d\mathbf{c}}{d\mathbf{l}} = f(\mathbf{c}) \\ \mathbf{c}(t_0) = \mathbf{c}_0 \end{cases}$$
 (3.1)

with $c(t), c_0 \in \mathbb{R}^n$ and $f: \mathbb{R}^n \to \mathbb{R}^n$, $f = (f_1, f_2, \dots f_n)^T$.

One step from t_0 to t_1 with $h=t_1-t_0$ of a 2-stage Rosenbrock method as presented in [16] reads:

$$\left(\frac{1}{\gamma_{11}h}I - J_0\right) \mathbf{k}_1 = f(\mathbf{c}_0) \tag{3.2}$$

$$\left(\frac{1}{\gamma_{22}h}I - J_0\right)\mathbf{k}_2 = f(\mathbf{c}_0 + \alpha\mathbf{k}_1) + \frac{\beta}{h}\mathbf{k}_1 \tag{3.3}$$

$$c_1 = c_0 + m_1 k_1 + m_2 k_2 (3.4)$$

where J_0 is the Jacobian matrix of f evaluated at c_0 , $J_0 = (\frac{\partial f_i}{\partial c_j})_{ij}|_{\mathbf{c}=\mathbf{c}_0}$ and the coefficients $\gamma_{11}, \gamma_{22}, \alpha, \beta, m_1, m_2$ are chosen to obtain a desired order of consistency and numerical stability. Since of special interest are the methods that require only one LU decomposition of $\frac{1}{\gamma_{ii}h}I - J_0$ per step, we consider the case when $\gamma_{11} = \gamma_{22} = \gamma$.

For the adjoint computations we have from (3.2), (3.3):

$$\left(\frac{\partial \mathbf{k}_1}{\partial \mathbf{c}_0}\right)^T = \left(J_0^T + \left(\frac{\partial J_0}{\partial \mathbf{c}_0} \times \mathbf{k}_1\right)^T\right) \left(\left(\frac{1}{\gamma h}I - J_0\right)^T\right)^{-1} \tag{3.5}$$

$$\left(\frac{\partial \mathbf{k}_2}{\partial \mathbf{c}_0}\right)^T = \left((I + \alpha \frac{\partial \mathbf{k}_1}{\partial \mathbf{c}_0})^T J_1^T + \frac{\beta}{h} (\frac{\partial \mathbf{k}_1}{\partial \mathbf{c}_0})^T + \left(\frac{\partial J_0}{\partial \mathbf{c}_0} \times \mathbf{k}_2\right)^T\right) \left((\frac{1}{\gamma h}I - J_0)^T\right)^{-1}$$

where J_1 is the Jacobian evaluated at $c_0 + \alpha k_1$, and the terms $(\frac{\partial J_0}{\partial C_0} \times k_i)$, i = 1, 2 are $n \times n$ matrices whose j column is $(\frac{\partial J_0}{\partial C_0^j})k_i$, i = 1, 2. We want to stress here the fact that these matrices are not symmetric and we will return to the computation of these terms later. Using (3.4, 3.5), for an arbitrary seed vector $u \in R^n$ we have:

$$\left(\frac{\partial \mathbf{c}_{1}}{\partial \mathbf{c}_{0}}\right)^{T} \mathbf{u} = \mathbf{u} + m_{1} \left(J_{0}^{T} + \left(\frac{\partial J_{0}}{\partial \mathbf{c}_{0}} \times \mathbf{k}_{1}\right)^{T}\right) \left(\left(\frac{1}{\gamma h}I - J_{0}\right)^{T}\right)^{-1} \mathbf{u} +
+ m_{2} \left(\left(I + \alpha \left(\frac{\partial \mathbf{k}_{1}}{\partial \mathbf{c}_{0}}\right)^{T}\right) J_{1}^{T} + \frac{\beta}{h} \left(\frac{\partial \mathbf{k}_{1}}{\partial \mathbf{c}_{0}}\right)^{T} + \left(\frac{\partial J_{0}}{\partial \mathbf{c}_{0}} \times \mathbf{k}_{2}\right)^{T}\right) \left(\left(\frac{1}{\gamma h}I - J_{0}\right)^{T}\right)^{-1} \mathbf{u}$$

To avoid frequent recomputations and to exploit the particular properties of the method, the order of the operations in the formula above become important. Below we present an efficient algorithm.

Step 1. Solve for v the linear system $(\frac{1}{\gamma h}I - J_0)^T v = u$. Then,

$$\left(\frac{\partial \mathbf{c}_{1}}{\partial \mathbf{c}_{0}}\right)^{T} \mathbf{u} = \mathbf{u} + m_{1} \left(J_{0}^{T} + \left(\frac{\partial J_{0}}{\partial \mathbf{c}_{0}} \times \mathbf{k}_{1}\right)^{T}\right) \mathbf{v} + m_{2} J_{1}^{T} \mathbf{v} + m_{2} \left(\frac{\partial \mathbf{k}_{1}}{\partial \mathbf{c}_{0}}\right)^{T} (\alpha J_{1}^{T} + \frac{\beta}{h} I) \mathbf{v} + m_{2} \left(\frac{\partial J_{0}}{\partial \mathbf{c}_{0}} \times \mathbf{k}_{2}\right)^{T} \mathbf{v} + m_{2} \left(\frac{\partial J$$

Step 2. Compute $\omega = J_1^T(m_2 v)$; $\omega_1 = \alpha \omega + \frac{m_2 \beta}{h} v$. Using (3.5) we get next:

Step 3. Solve for θ the linear system $(\frac{1}{\gamma h}I - J_0)^T\theta = \omega_1$.

After replacing in (3.6), it results:

$$\left(\frac{\partial \mathbf{c}_{1}}{\partial \mathbf{c}_{0}}\right)^{T} \mathbf{u} = \mathbf{u} + m_{1} \left(J_{0}^{T} + \left(\frac{\partial J_{0}}{\partial \mathbf{c}_{0}} \times \mathbf{k}_{1}\right)^{T}\right) \mathbf{v} + \omega + \left(J_{0}^{T} + \left(\frac{\partial J_{0}}{\partial \mathbf{c}_{0}} \times \mathbf{k}_{1}\right)^{T}\right) \theta + m_{2} \left(\frac{\partial J_{0}}{\partial \mathbf{c}_{0}} \times \mathbf{k}_{2}\right)^{T} \mathbf{v} \tag{3.7}$$

and after arranging the terms we obtain:

Step 4. Compute
$$\left(\frac{\partial \mathbf{c}_1}{\partial \mathbf{c}_0}\right)^T \mathbf{u} =$$

$$\mathbf{u} + \omega + J_0^T(m_1\mathbf{v} + \theta) + (\frac{\partial J_0}{\partial c_0} \times \mathbf{k}_1)^T(m_1\mathbf{v} + \theta) + m_2(\frac{\partial J_0}{\partial c_0} \times \mathbf{k}_2)^T\mathbf{v}$$
(3.8)

In formula (3.7) it appears that a routine to compute the product $J_0^T s$ (s a seed vector) must be called twice: first with the seed vector $m_1 \mathbf{v}$, second with the seed vector θ . From (3.8) it results that is enough to call the routine once, with the seed vector $m_1 \mathbf{v} + \theta$. The same observation is made for the products $(\frac{\partial J_0}{\partial \mathbf{C}_0} \times \mathbf{k}_1)^T m_1 \mathbf{v}$, $(\frac{\partial J_0}{\partial \mathbf{C}_0} \times \mathbf{k}_1)^T \theta$. We now focus on the terms of the form $(\frac{\partial J_0}{\partial \mathbf{C}_0} \times \mathbf{k})^T \mathbf{v}$ whose evaluation dominate the computational cost of the algorithm given by Step 1-4. Here \mathbf{k} , $\mathbf{v} \in \mathbb{R}^n$ are arbitrary constant vectors. For the i component we have:

$$\left(\left(\frac{\partial J_0}{\partial c_0} \times \mathbf{k} \right)^T \mathbf{v} \right)_i = \left(\frac{\partial J_0}{\partial c_0^i} \mathbf{k} \right)^T \mathbf{v} = \mathbf{k}^T \left(\frac{\partial (J_0^T \mathbf{v})}{\partial c_0^i} \right) = \left(\frac{\partial (J_0^T \mathbf{v})}{\partial c_0^i} \right)^T \mathbf{k} \tag{3.9}$$

Consider now the function $g:R^n\to R^n$, $g(c_0)=J_0^T v$. Observe that the Jacobian matrix of g is symmetric. We have

$$g(c_0) = \left(\sum_{l=1}^n J_{0,(l,1)} v_l, \dots, \sum_{l=1}^n J_{0,(l,n)} v_l\right)^T$$

which gives for the (i,j) entry in the Jacobian matrix:

$$\frac{\partial g_i(\mathbf{c}_0)}{\partial \mathbf{c}_0^j} = \sum_{l=1}^n \left(\frac{\partial^2 f_l}{\partial \mathbf{c}_0^i \partial \mathbf{c}_0^j} \right) \mathbf{v}_l = \sum_{l=1}^n H_{f_l}(i,j) \mathbf{v}_l$$

where H_{f_l} is the Hessian matrix of the function $f_l: \mathbb{R}^n \to \mathbb{R}$.

Then $\frac{\partial g(\mathbf{C}_0)}{\partial \mathbf{C}_0} = \sum_{l=1}^n H_{f_l} \mathbf{v}_l$, so $\frac{\partial g(\mathbf{C}_0)}{\partial \mathbf{C}_0}$ is symmetric. Using (3.9) it results:

$$\left(\left(\frac{\partial J_0}{\partial c_0} \times \mathbf{k} \right)^T \mathbf{v} \right) = \left(\frac{\partial g(c_0)}{\partial c_0} \right) \mathbf{k}$$
 (3.10)

The symmetry of the Jacobian matrix of the function g used in relation (3.10) plays a significant role in the implementation of the adjoint code which we present next.

ii) Implementation of the adjoint code. The forward integration of problem (3.1) using implicit methods together with the performance analysis is given in [27, 28, 34], proving that when the sparsity of the system is efficiently exploited Rosenbrock methods outperform traditional explicit methods like QSSA and CHEMEQ. Implementation is done in the symbolic kinetic preprocessor KPP environment [9] which generates the sparse matrix factorization LU required in (3.2, 3.3) with a minimal fill-in [26] and the routine to forward-backward solve the linear systems without indirect adressing. One step of the adjoint code (from t_1 to t_0) requires a forward run from t_0 to t_1 given by the formulas (3.2-3.4) followed by the pure adjoint computations given by Step1-4. It is important to notice that the LU decomposition accounts for most of the CPU time of the code, and there is no need to repeat it during the pure backward integration.

With the LU decomposition of $(\frac{1}{\gamma h}I - J_0)$ available from (3.2), $Step\ 1$ reads: $U^TL^Tv = u$. A new loop free routine is generated by KPP for forward-backward solving this system in sparse format avoiding indirect addressing. The computational cost of $Step\ 1,3$ can be then compared with the corresponding part from (3.2) and (3.3).

Step 2 requires evaluation of the product $J_1^T v$ which is automatically computed by KPP using sparse multiplications. This introduces some extra work (J_1 is evaluated at $c_0 + \alpha k_1$), but its cost is relatively cheap. The efficiency of the adjoint code is then dominated by the implementation of Step 4, given by the formula (3.8). The computation of the terms of the form $(\frac{\partial J_0}{\partial C_0} \times k)^T v$ in formula (3.8) appears to require the order: forward automatic mode to compute $J_0 k$, reverse mode to compute $(\frac{\partial J_0}{\partial C_0} \times k)^T v$. Relation (3.10) can be used to rewrite (3.8) as:

$$\left(\frac{\partial c_1}{\partial c_0}\right)^T u = u + \omega + g_1(c_0) + \left(\frac{\partial g_1(c_0)}{\partial c_0}\right) k_1 + m_2 \left(\frac{\partial g_2(c_0)}{\partial c_0}\right) k_2$$
 (3.11)

with
$$g_1, g_2: \mathbb{R}^n \to \mathbb{R}^n$$
, $g_1(c_0) = J_0^T(m_1 v + \theta)$, $g_2(c_0) = J_0^T v$.

The functions g_1, g_2 are generated via KPP, taking full advantage of the sparsity of the

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Jacobian matrix J_0 . In (3.11) we have then to compute the $Jacobian \cdot vector$ products for the functions g_1, g_2 which can be done by forward automatic differentiation [2, 14]. The cost is 2-3 times the cost of evaluating $g_1(c_0), g_2(c_0)$ and remains low due to the sparse structure of J_0 . This leads to a considerable saving in CPU time. By default, during the computation of $Jacobian \cdot vector$ products, forward automatic differentiation computes the value of the function. Automatic differentiation for g_1 provides then the value $g_1(c_0)$ and there is no need to compute it separately. Last but not least, the computations related to g_1 and g_2 are independent allowing parallel implementation.

4. PERFORMANCE AND VALIDATION OF THE ADJOINT ALGORITHM

The algorithm and implementation presented in Section 3 have the benefit that the adjoint part of the chemistry integration is generated completely automatically, taking full advantage of the sparsity of the system. This allows the user to easily move from one model to another and makes it very attractive compared with the hand written codes which construction for large models can be a difficult process. Moreover since symbolic computations are used, rounding errors are avoided and the accuracy of the results goes up to the machine precision. Implementation in the KPP context has also the advantage that avoids the introduction of auxiliary adjoint variables which has direct impact on the performance of the code both in terms of memory usage and CPU time.

As a particular case we consider the 2^{nd} order 2-stage Rosenbrock method ROS2 which is obtained from (3.2-3.4) by taking $\alpha = \frac{1}{\gamma}$, $\beta = -\frac{2}{\gamma}$, $m_1 = \frac{3}{2\gamma}$, $m_2 = \frac{1}{2\gamma}$. Choosing $\gamma = 1 \pm 1/\sqrt{2}$ the method is L-stable and the numerical experiments presented in this section were performed with $\gamma = 1 + 1/\sqrt{2}$. The superior stability, positivity and conservation properties of this scheme are analyzed by *Verwer et al.* [34] who reports good results in the context of various types of operator splitting even when large fixed step sizes (10 to 20 min.) are used.

i) The box model. In order to test the performance of the implementation we consider first a box model for the problem (1.1). The chemistry part is based on the Carbon Bond

Mechanism IV (CBM-IV, [13]) with 32 chemical species involved in 70 thermal and 11 photolytic reactions. The data assimilation problem is set using the "twin experiments method", with the background term dropped and the logarithmic form of (1.3). Taking the logarithm of the concentrations has the advantage that the positivity constraint is eliminated and scales the system. The minimization routine used is the Quasi-Newton limited memory L-BFGS algorithm [4, 5], anticipating extension to large scale models. The initial concentrations follow the urban scenario as described in [27], with an initial concentration of 70 ppb for O3. Assimilation starts at the beginning of the third day (6:00 LT) over a period of 6 hours, with measurements provided every 15 minutes. As the initial guess for the concentrations we choose the values at the beginning of the second day. The one day period is introduced in order to allow the system to equilibrate. The integration is restarted every 15 minutes with a minimum stepsize of 1 sec., simulating an operator splitting environment. With the absolute and relative tolerances Atol = 1 molec., Rtol = 0.01, the number of intermediate steps within a 15 min interval ranges from 5 to 12, providing a relatively short forward trajectory. Two experiments were performed: in Run 1 measurements were provided for ozone only, and in Run 2 for ozone and NO2. The results of the assimilation for O3, NO2, and NO are shown in Figure 1. It can be seen that model predictions are highly improved even after the end of the assimilation window (12:00 LT), and introducing NO2 measurements is of benefit not only for the NO2 and NO analysis, but also for the O3 analysis. However, since additional constraints are introduced, this increases the number of iterations in the optimization (Table I).

As an alternative way to compute the gradients we use the second order central difference formula [1] with $\epsilon = (2.22 \times 10^{-16})^{1/3}$. Figure 2 (left Run 1, right Run 2) shows the relative and absolute differences between the computed gradients with respect to some important species in the model. Since in the context of stiff computations and a long trajectory the roundoff errors can highly affect the accuracy of the difference schemes, we also show in Figure 3 the corresponding results for assimilation with only one measurement, at T = 6:15 LT, together with the computed gradients. In average 8 to 10 significant digits of

the gradients are matched (when $\nabla \mathcal{F}$ is nearly zero, the relative error size in the gradient approximation for difference schemes may become very large [1]).

For consistency with the implementation for large scale models, where the storage of the entire trajectory is not a realistic option, a checkpointing scheme is applied for the gradient computations. First, a full forward run is used to store the states of the system at the measurement moments. Second, during the backward integration, a full forward run stores the trajectory between measurements (see Section 1) and information about the stepsize used. Third, the computations given by Step 1-4 in Section 3 are performed (pure backward integration). Observe that the numerical values of k_1, k_2 are still required. These recomputations may be avoided by storing all k1 during the second forward run, but this will double its storage requirements. We prefer to repeat (3.2) to compute k_1 , then avoid (3.3) by setting $m_2 k_2 = c_1 - c_0 - m_1 k_1$ in (3.11). The technical report of the optimization process is outlined in Table I (Run 1,2). We denote by KPP-AD the implementation of the adjoint code using the KPP generated adjoint routines and forward automatic differentiation. It can be seen that the average ratio between the CPU time required to compute the gradient (and cost function value) and the CPU time of a forward run is about 3.7, which gives an average ratio $cpu(pure\ backward\ integration + (3.2))/cpu(forward\ integration) \approx 1.7$. This makes our implementation very efficient.

As an alternative way for automatic adjoint code generation, we applied the adjoint model compiler TAMC [14, 15] to (3.2-3.4) using the same checkpointing scheme. In particular, we noticed that the adjoint compiler fails to generate an efficient adjoint code for the sparse chemistry computations. The timing results included in Table I (TAMC) were obtained with significant user intervention, in order to reduce the frequent recomputations generated by the adjoint compiler.

ii) Application to a 1-D problem. We consider now a one dimensional horizontal test problem corresponding to (1.1). The wind field and the diffusion coefficient are taken constant, $\mathbf{u}=10$ km/hour (left-to-right), $K=10^{-3}\mathrm{Km}^2/\mathrm{sec}$. Second order Strang

splitting is applied:

$$c(t_{n+1}) = \overline{F}_A\left(t_{n+\frac{1}{2}}, \frac{h}{2}\right) \overline{F}_R(t_n, h) \overline{F}_A\left(t_n, \frac{h}{2}\right) c(t_n)$$

with a splitting interval $t_{n+1}-t_n=15$ min. The advection operator is discretized using a limited k = 1/3 upwind flux interpolation as presented in [17], and the diffusion operator using central differences formula. Together they define F_A . The numerical method defining \overline{F}_A is the explicit trapezoidal rule. Concentrations are kept constant at the left boundary (x=0) and at the right boundary we consider $\frac{\partial \mathbf{c}}{\partial n}=0$. For a full description of the space discretization the reader should consult [25]. With the spatial domain [0,500] Km and a uniform grid $\Delta x = 5$ Km, the dimension of the corresponding (1.2) problem is 3200. A highly polluted region is considered between 200 and 300 Km, with initial concentrations and emissions as for the urban scenario and for the rest of the domain rural concentrations and emissions are provided [27]. Emissions take place at constant rate, and are included in F_R . Interpolation is done between the center (250 Km) and the urban limits. In order to allow the system to equilibrate, box models (chemistry only) are integrated for one day over the whole grid. The results are the "true" initial conditions, c_0^{ref} . "Measurements" are then generated every 15 min by a 6 hours transport-chemistry run. Figure 4 shows the spatial distribution of the reference concentrations at the beginning (6:00 LT) and at the end (12:00 LT) of the assimilation interval for O3 and NO2. First guess initial concentrations are generated similar to c_0^{ref} , but with an uniform injection of 0.1 ppb/hour over the rural area and 0.5 ppb/hour over the urban area of NO_x during the box models integration, which accounts for an error in emission estimates. Assimilation starts at 6:00 LT over a six hour interval, with measurements for ozone every 15 min. and for NO2 each hour, at all grid points. A checkpointing strategy is applied for the gradient computations. First, a full forward run is used to store the states of the model after each operator splitting interval. Second, for the backward integration, a forward run stores the states within a splitting interval (1 + all chemistry steps). Third, the pure backward integration is performed, where the intermediate states within transport and within the chemistry steps need to be provided

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by a simplified forward run. The adjoint part of the advection- diffusion equations is automatically generated using TAMC. The computational scheme for one split interval is described in Figure 5. The performance of the optimization process is given in Table I (Run 3, KPP-AD) and the assimilation results are presented in Figure 6. We note here that the previous timing results for the adjoint code are recovered, confirming the success of the implementation. The results obtained with TAMC applied for full transport-chemistry adjoint computations are also included in Table I (Run 3, TAMC).

5. CONCLUSIONS AND FURTHER WORK

The development of powerful computing machines in the past decade made the variational data assimilation technique for large scale models an intensive explored area. With a dimension of the systems of order 10⁶ any attempt to provide the gradient of the cost function using a direct method (finite differences, solving the sensitivity systems) is not feasible, and the adjoint approach is an attractive alternative. In the context of stiff chemical equations explicit integrators may take prohibitive small stepsize (or just fail), which highly affects the performance of the adjoint code.

While several adjoint models for explicit or semi-implicit numerical methods have been constructed, implementation of implicit methods remains a delicate problem. In this paper we introduced the adjoint computations and an efficient implementation of the 2-stage Rosenbrock methods which is suitable for automatization and parallel coding. The algorithm and the properties we described can easily be generalized to s-stage methods and it is of interest to analyze how this implementation can be applied to implicit Runge-Kutta methods [16]. Further work includes testing on comprehensive models, extension of the set of control variables to include the emission field and depositions, implementation in the context of W-transformation and different types of operator splitting as well as the possibility to use approximate gradients.

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Figure captions

Fig.1 Assimilation takes place from 6 to 12 LT. Measurements are provided every 15 min for O3 only in Run 1 (left), and for O3 and NO2 in Run 2 (right). Solid line with dots = reference run; solid line = assimilation result; dotted line = first guess.

Fig.2 Absolute (solid line) and relative (dotted line) differences between the computed gradients using the central difference formula and automatic adjoint computations during the optimization process. Left-Run 1, right-Run 2.

Fig.3 Absolute (dashed line) and relative (dotted line) differences between the computed gradients (solid line) using the central difference formula and automatic adjoint computations. Left-Run 1, right-Run 2. To reduce the roundoff errors a short assimilation interval (15 min) is considered.

Fig.4 Spatial distribution of the reference concentrations for O3 and NO2. Solid line = initial(LT=6:00), dotted line = final (LT=12:00). High NO_x emissions take place in the urban area (200 - 300 Km).

Fig.5 Computational scheme of the adjoint code for one time split interval. Concentrations are stored after each step during the forward integration, then loaded for the adjoint integration. Additional partial forward computations are required during the adjoint integration.

Fig.6 Assimilation results at some representative points for each area. First line O3, second NO2, third NO. Solid dots= true solution, solid line= assimilation result, dotted line= first guess solution.

 $\label{eq:TABLE I} \mbox{ \begin{tabular}{ll} \label{eq:TABLE I} \end{tabular} } \mbox{ \begin{tabular}{ll} \label{eq:TABLE I} \end{tabular}$ Performance of the optimization process and the adjoint code \$^a\$. } \mbox{ \end{tabular}

				~cpu/iter		$\sim \mathrm{cpu}(\mathcal{F} + \nabla \mathcal{F})/\mathrm{cpu}(\mathcal{F})$		
Run	Iter.	$(\mathcal{F}, \nabla \mathcal{F})$ -eval.	\sim cpu (\mathcal{F})	KPP-AD	TAMC	$KPP ext{-}AD^b$	$TAMC^b$	\mathcal{F} init $/\mathcal{F}$ end
1.	27	32	0.017	0.35	0.42	3.66	7.71	1.e5
2.	32	38	0.017	0.36	0.44	3.71	7.75	2.8e3
3. ^c	34	34	2.05	8.32	16.6	3.65	7.69	1.e2

a All the computations were done on a HP-UX B.10.20 A 9000/778 machine with level 2 optimization. The
 CPU time is in seconds.
 b The time to read-write data to files is not considered for these ratios.
 c Simplified recomputations for the advection-diffusion part are taken during the backward integration (see Fig. 5).

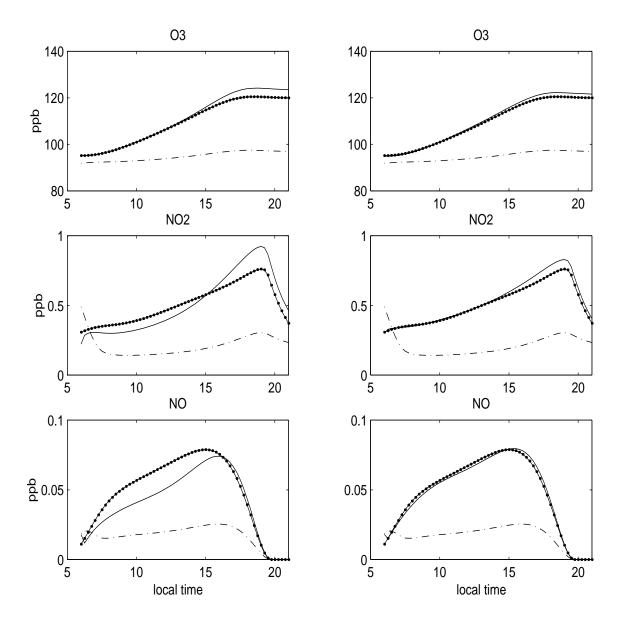


FIGURE 1

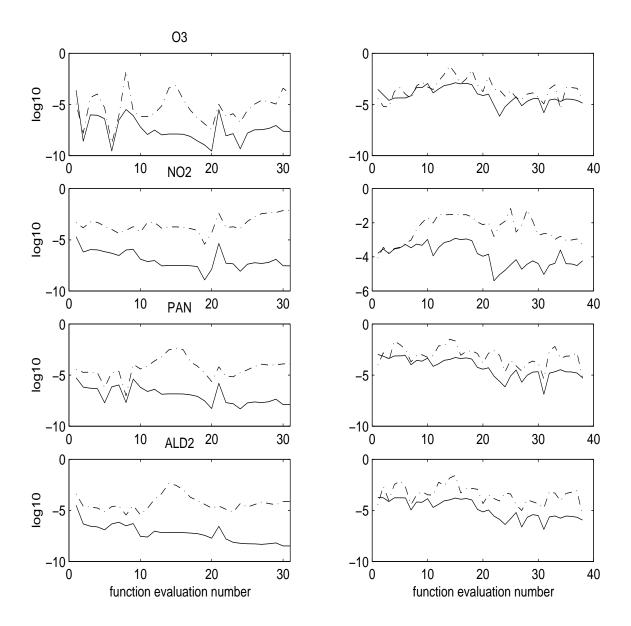


FIGURE 2

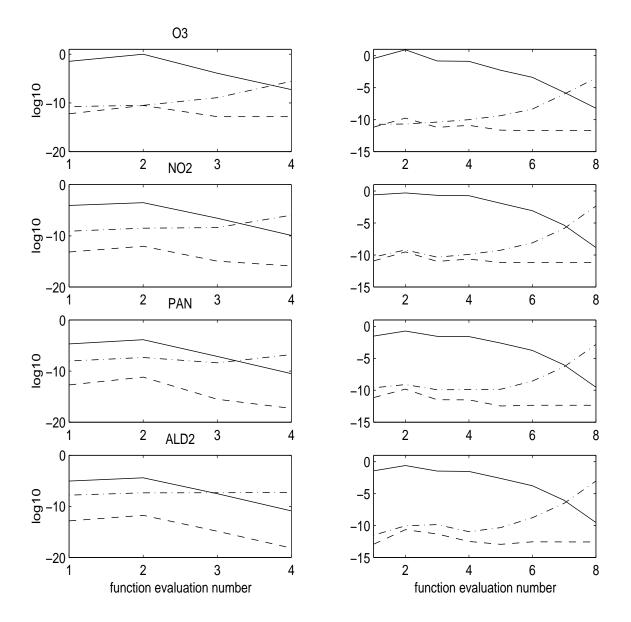


FIGURE 3

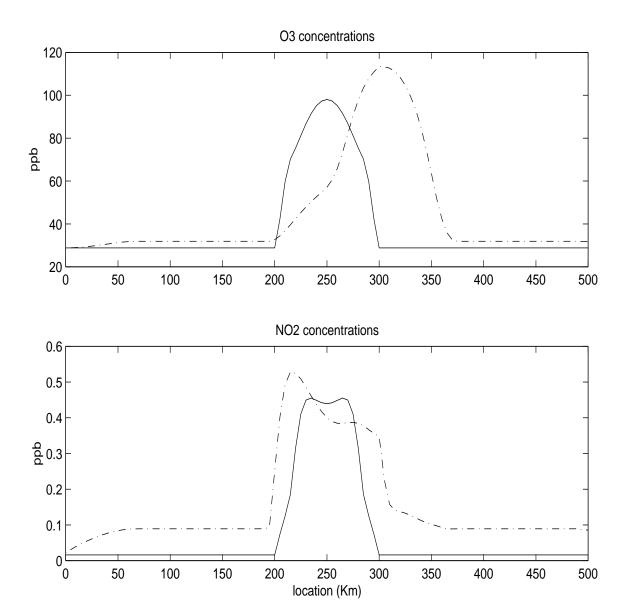


FIGURE 4

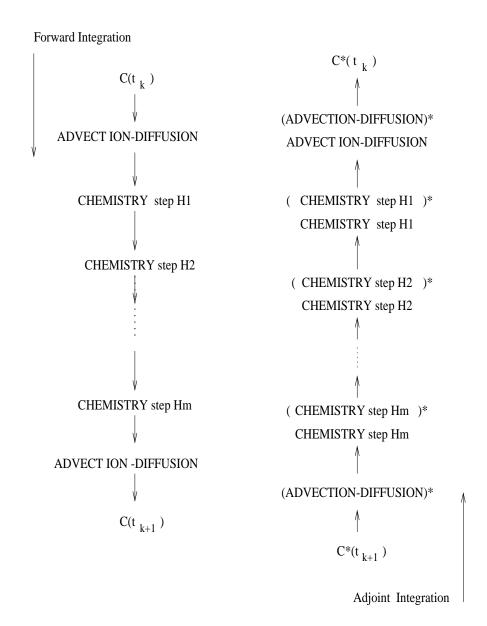


FIGURE 5

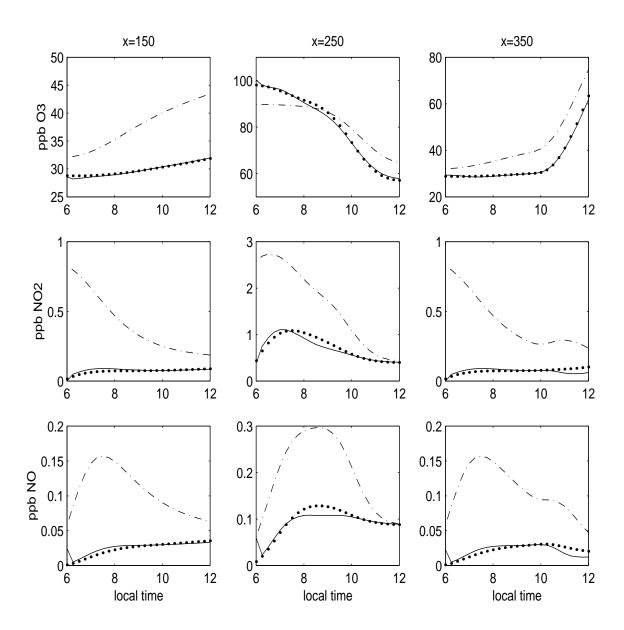


FIGURE 6